FUNDAMENTALS OF FLUID MECHANICS

MMI103

Lesson 2 (course and exercices)

Thursday 18th september 2025

MASS CONSERVATION (reminder; Lesson 1)

• global equivalent formulations

$$\frac{d}{dt} \int_{\mathcal{D}(t)} \rho d\Omega = 0, \quad \frac{\delta}{\delta t} \int_{\mathcal{D}} \rho(\underline{x}, t) d\Omega = -\int_{\partial \mathcal{D}} \rho \underline{u} . \underline{n} da$$

• local equivalent formulations (where the flow is smooth)

$$\frac{d\rho}{dt} + \rho \operatorname{div}(\underline{u}) = 0, \quad \frac{\partial \rho}{\partial t} + \operatorname{div}(\rho \underline{u}) = 0, \quad \frac{dg}{dt} = \frac{\partial g}{\partial t} + \underline{grad}[g].\underline{u}$$

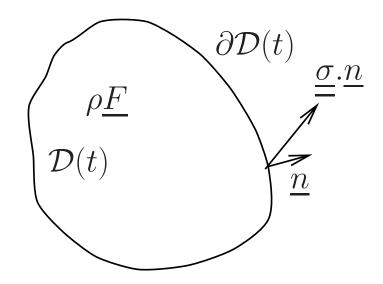
• Incompressible flow?

$$\frac{d\rho}{dt} = 0, \quad \operatorname{div}(\underline{u}) = 0$$

 \bullet new useful identity for f a specific quantity and a smooth flow

$$F = \rho f, \quad \frac{d}{dt} \int_{\mathcal{D}(t)} \rho f d\Omega = \int_{\mathcal{D}(t)} \rho \left[\frac{df}{dt}\right] d\Omega$$

GLOBAL MOMENTUM CONSERVATION LAW



$$\frac{d}{dt} \int_{\mathcal{D}(t)} \rho \underline{u} d\Omega = \int_{\mathcal{D}(t)} \rho \underline{F} d\Omega + \int_{\partial \mathcal{D}(t)} \underline{\underline{\sigma}} \underline{n} da$$

- Valid also if there is an inert surface $\Sigma(t)$ of discontinuities of $\rho \underline{u}$ inside the domain $\mathcal{D}(t)$
- \underline{F} : specific (i.e. per unit mass) body force
- \underline{F} must include the inertial body forces if the frame of reference is not Galilean (see later)
- Examples: $\underline{F} = g$ for gravity, $\underline{F} = -grad[\Phi]$ when conservative and deriving from the potential Φ
- $\underline{\underline{\sigma}}$ is the so-called Cauchy stress tensor. It is expressed in terms of (ρ, p, \underline{u}) by the fluid rheological law. Its Cartesian components are σ_{ij} and $\underline{\underline{\sigma}}.\underline{n} = (\sigma_{ij}n_j)\underline{e}_i$

OBTAINED EQUIVALENT FORMS TAKEN BY A GLOBAL CONSERVATION LAW

General case of a moving domain

$$\frac{\delta}{\delta t_V} \int_{\mathcal{D}(t)} F(\underline{x}, t) d\Omega = \int_{\mathcal{D}} P_F(\underline{x}, t) d\Omega - \int_{\partial \mathcal{D}} [F(\underline{u} - \underline{V}) - \underline{A}] \underline{n} da$$

Steady domain

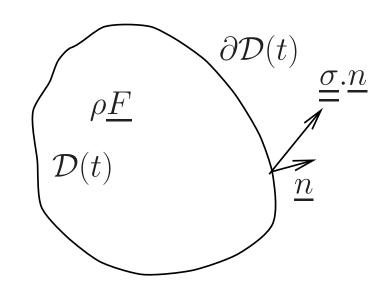
$$\frac{\delta}{\delta t} \int_{\mathcal{D}} F(\underline{x}, t) d\Omega = \int_{\mathcal{D}} P_F(\underline{x}, t) d\Omega - \int_{\partial \mathcal{D}} (F\underline{u} - \underline{A}) \underline{n} da$$

Material domain

$$\frac{d}{dt} \int_{\mathcal{D}(t)} F(\underline{x}, t) d\Omega = \int_{\mathcal{D}(t)} P_F(\underline{x}, t) d\Omega + \int_{\partial \mathcal{D}(t)} \underline{A} \cdot \underline{n} da$$

Hold even in presence of a surface of discontinuities $\Sigma(t)$ INERT for the quantity \mathcal{F}

OTHER GLOBAL AND LOCAL MOMENTUM CONSERVATION FORMULATIONS



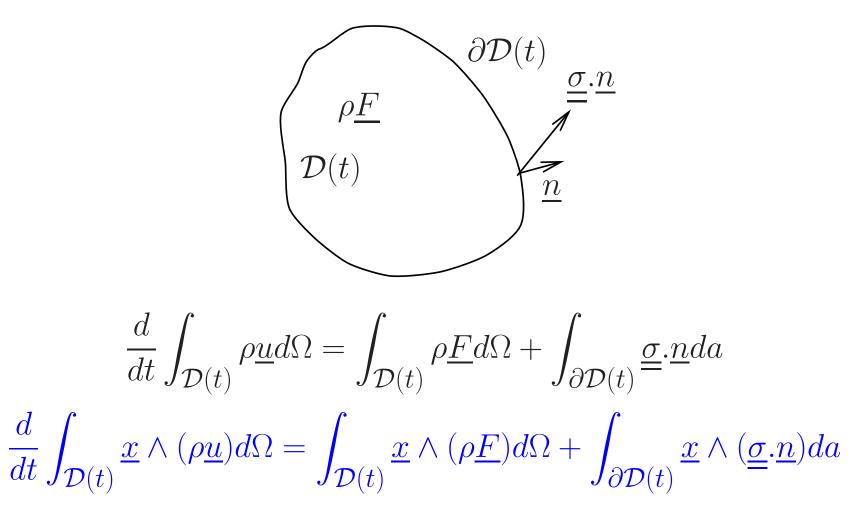
$$\frac{\delta}{\delta t} \int_{\mathcal{D}} \rho \underline{u} d\Omega = \int_{\mathcal{D}} \rho \underline{F} d\Omega + \int_{\partial \mathcal{D}} [\underline{\underline{\sigma}} \underline{\cdot} \underline{n} - \rho(\underline{u} \underline{\cdot} \underline{n}) \underline{u}] da$$

$$\rho \frac{d\underline{u}}{dt} = \rho \underline{F} + \text{div}(\underline{\underline{\sigma}}), \quad \text{div}(\underline{\underline{\sigma}}) = \sigma_{ij,j} \underline{e}_{i}$$

Recall that

$$\frac{d\underline{u}}{dt} = \frac{\partial \underline{u}}{\partial t} + \underline{grad}[u^2/2] + \underline{rot}(\underline{u}) \wedge \underline{u}, \qquad \sigma_{ij,j} = \frac{\partial \sigma_{ij}}{\partial x_j}$$

ANGULAR MOMENTUM CONSERVATION LAW?



For a symmetric stress tensor $\underline{\underline{\sigma}}$ (which means $\sigma_{ij} = \sigma_{ji}$) the second identity is induced by the momentum conservation law!

IN SUMMARY

- 5 unknown Eulerian fields: ρ, p, \underline{u}
- \bullet $\underline{\sigma}$ symmetric. True for most encountered fluids
- $\underline{\sigma}$ provided versus (ρ, p, \underline{u}) from the fluid nature. \underline{F} is also supplied.
- ullet T and other thermodynamic variables deduced from (ρ, p) using the fluid equation of state
- Mass and momentum law conservations provide 4 equations

$$\frac{d\rho}{dt} + \rho \operatorname{div}(\underline{u}) = 0, \quad \rho \frac{d\underline{u}}{dt} = \rho \underline{F} + \operatorname{div}(\underline{\underline{\sigma}})$$

- In general one additional equation is still lacking at that stage.

 Provided by the energy conservation (due to thermodynamics, see later)
- In some cases mass and momentum conservation are sufficient. For instance: fluid at rest, homogeneous flowing fluid

DEFINITION OF A FLUID

- A fluid: medium which when at rest experiences no tangential stress
- For a fluid at rest

$$\underline{\underline{\sigma}}.\underline{\underline{n}} = -p\underline{\underline{n}}$$

with p the so-called pressure

NON-VISCOUS FLUID

• A fluid is non-viscous if even when flowing

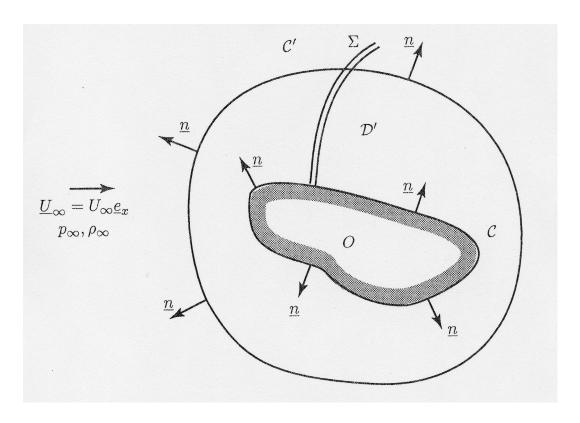
$$\underline{\underline{\sigma}}.\underline{\underline{n}} = -p\underline{\underline{n}}$$

• Example: a gas

ILLUSTRATING EXERCICES

- fluid at rest (stratified or homogeneous fluid)
- flowing non-viscous fluid (compressible or homogeneous)

Force exerted by a steady flow of a non-viscous fluid on a motionless body



$$\int_{\mathcal{D}'} \{p\underline{n}' + \rho(\underline{u}.\underline{n}')\underline{U}\} da = \underline{0}$$

$$\underline{R} = -\int_{\mathcal{C}'} \{p\underline{n} + \rho(\underline{u}.\underline{n})\underline{u}\} da$$

Requires the far-field behaviour of (ρ, p, \underline{u})

